

Additive Manufactured Foams for Power Electronics Thermal Management

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1.1 Wide-bandgap devices and motivation

- Wide-bandgap (WBG) devices have higher efficiencies, withstand higher breakdown voltages, can operate at increased switching frequencies, and function at higher temperatures
- Devices seeing mass commercialization and implementation in high voltage applications
- Design for WBG leads to miniaturization and potential hotspots
- Reexamination of thermal management needed for smaller devices and systems

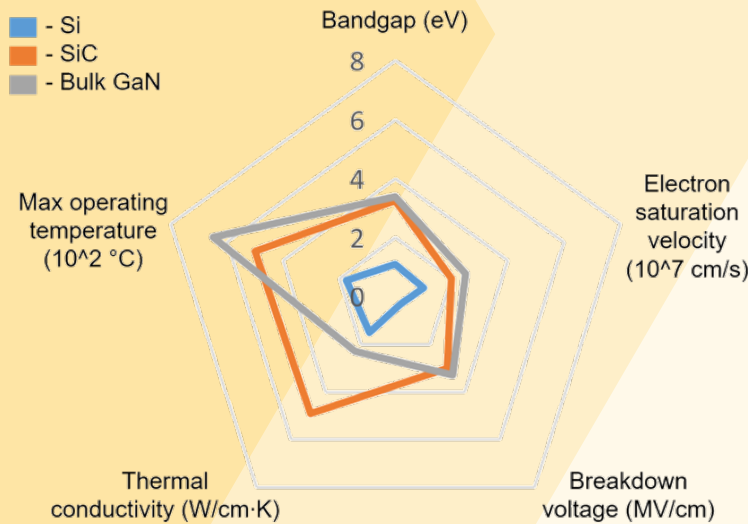
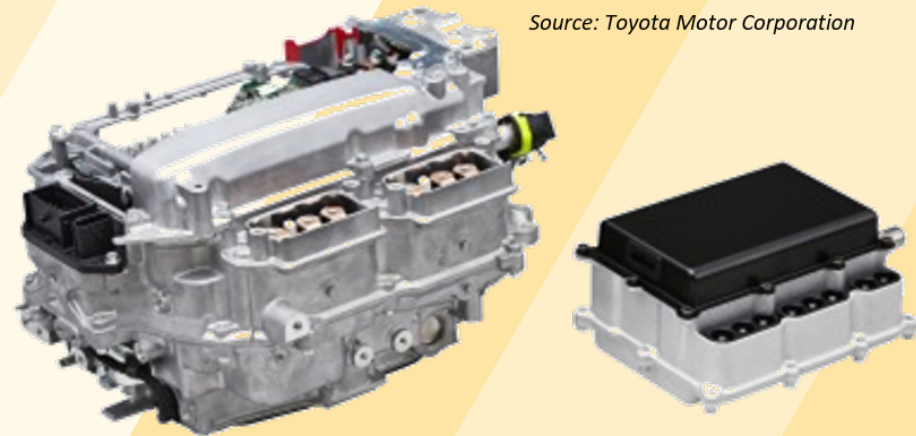


Figure 1: Material properties of power semiconductors



Source: Toyota Motor Corporation

Left: PCU with silicon power semiconductors (Production model)
Right: PCU with SiC power semiconductors (Future Target)

Figure 2: Miniaturization potential with system-level redesign using WBG devices

1.2 Metal foams and additive manufacturing

- Open-cell foams - interconnecting nodes and ligaments with high porosity, tortuous flow paths, and high specific surface area (SSA)
- Metal foams are used in applications ranging from catalysts for chemical reactions, impact absorption, and heat transfer
- Additive manufacturing (AM) has been used for foam-type structures, but not the combination between AM and metal foams is relatively unexplored
- Present work investigates the thermo-hydraulic performance of both traditionally manufactured metal foams and AM foams as a method of heat transfer enhancement

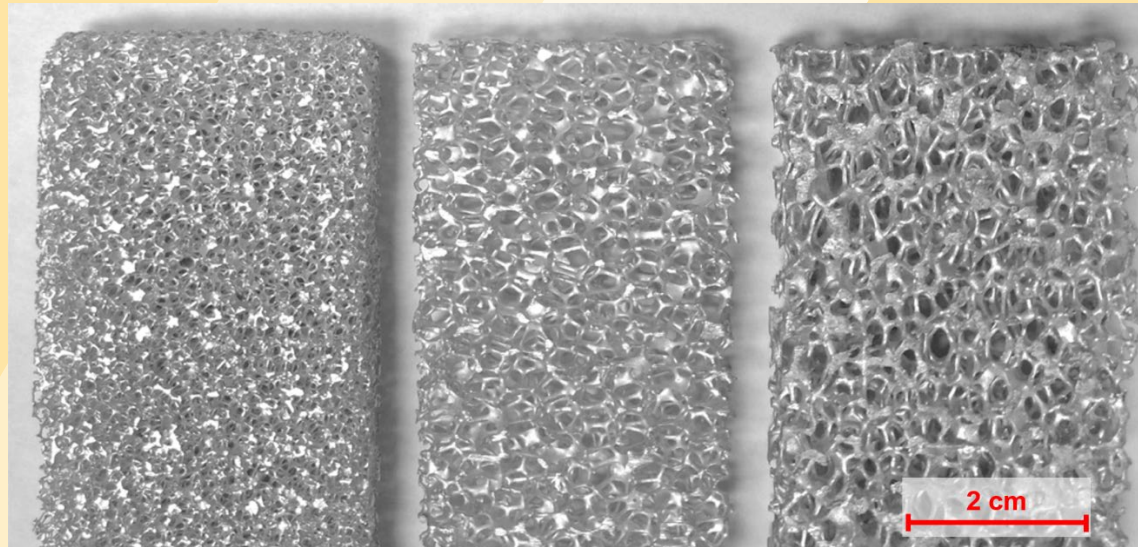


Figure 3: Photograph of metal foams of various sizes purchased from ERG Aerospace, Inc.

2.1 Characterization methodology, unit cell selection

- 5 PPI, processed from 6101 alloy, and underwent T6 heat treatment
- Zeiss Metrotom 800 for x-ray μ CT (scanned at 0.25° rotations, $18.43 \mu\text{m}$ voxel size)
- ImageJ/BoneJ used for image analysis

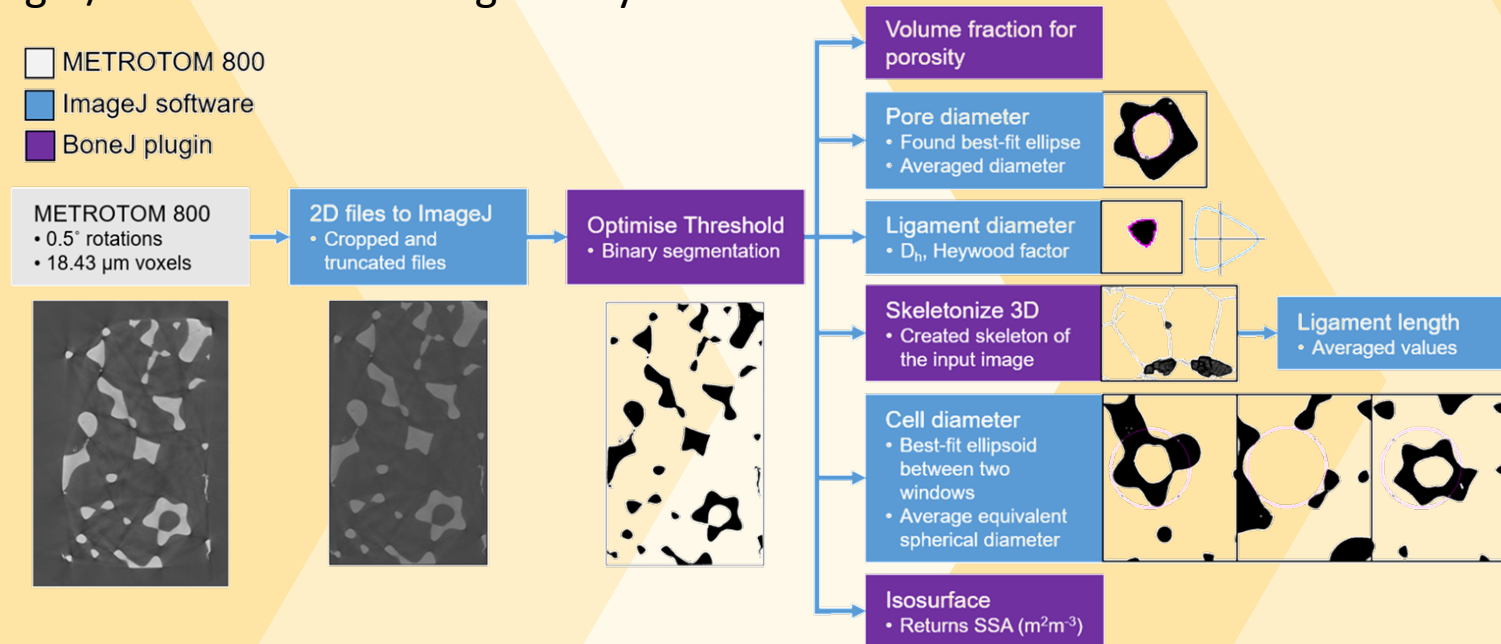


Figure 4: Illustration of steps for commercial stochastic foam characterization.

- Rhombic dodecahedron unit cell chosen for this work

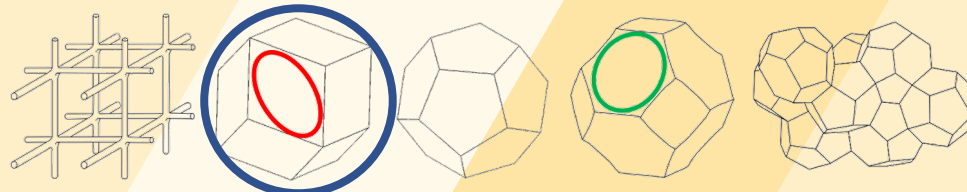


Figure 5: Types of unit cells seen in literature.

2.2 Unit cell description and experimental test samples

- AM unit cell seen in figure 4
- Unit cell based on porosity and cell diameter
- Reasonable agreement for most properties between result, literature, and rhombic dodecahedron unit cell
- ERG foam bonded with Omegabond 200 Epoxy Adhesive ($k = 1.38 \text{ W/m}\cdot\text{K}$, thickness 0.3 mm) to aluminum substrate

Table 1: Comparison of foam properties from x-ray μ CT analysis, literature, and AM foam.

Parameter	Result	Literature comparison	Rhombic dodecahedron
<i>PPI</i>	5	5	5
<i>Porosity</i>	86.5%	92%	86.5%
<i>Ligament diameter (mm)</i>	0.508	0.505	0.548
<i>Ligament length (mm)</i>	1.94	1.72	2.014
<i>Pore diameter (mm)</i>	2.58	2.61	1.35
<i>Cell diameter (mm)</i>	4.65	4.60	4.65
<i>Surface area (m^2m^{-3})</i>	571.1	510	927.35

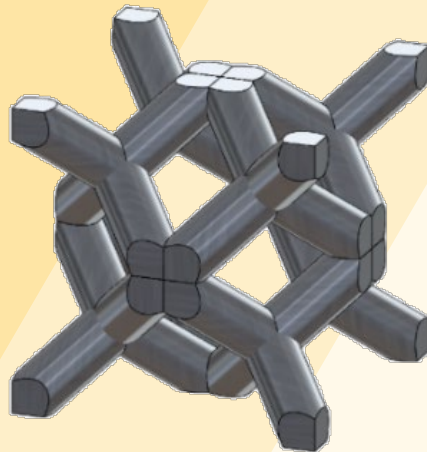


Figure 6: Dimetric and diagonal views of a rhombic dodecahedron based unit cell.

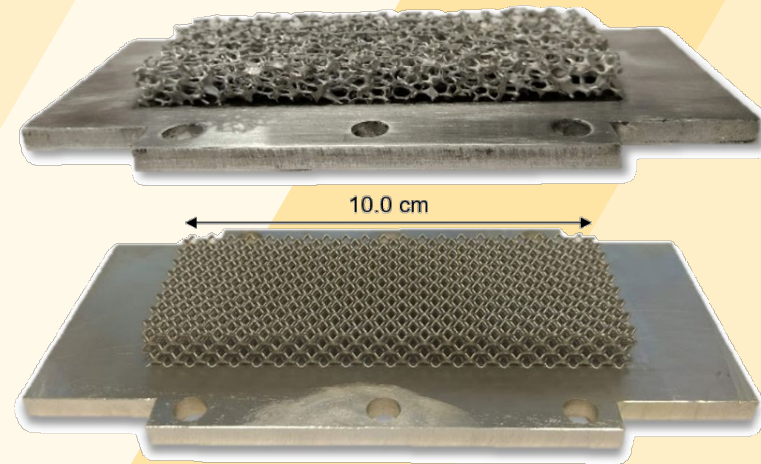


Figure 7: Stochastic ERG foam with visible thermal epoxy layer (top) and designed foam (bottom)

3.1 Computational model description and assumptions

- *Isosurface* command in ImageJ to export stochastic STL file
- Dimensions: 9.30 mm x 4.65 mm x 25.0 mm and 9.30 mm x 2.33 mm x 46.5 mm
- Assumptions:
 - Representative elementary volume (> 8 unit cells for REV)
 - Minimal inlet effects (valid at lower speeds)
 - Steady state, laminar ($Re_K = 37.5$), incompressible flow with negligible viscous dissipation
- Thermal resistance from thermal epoxy included into simulation results

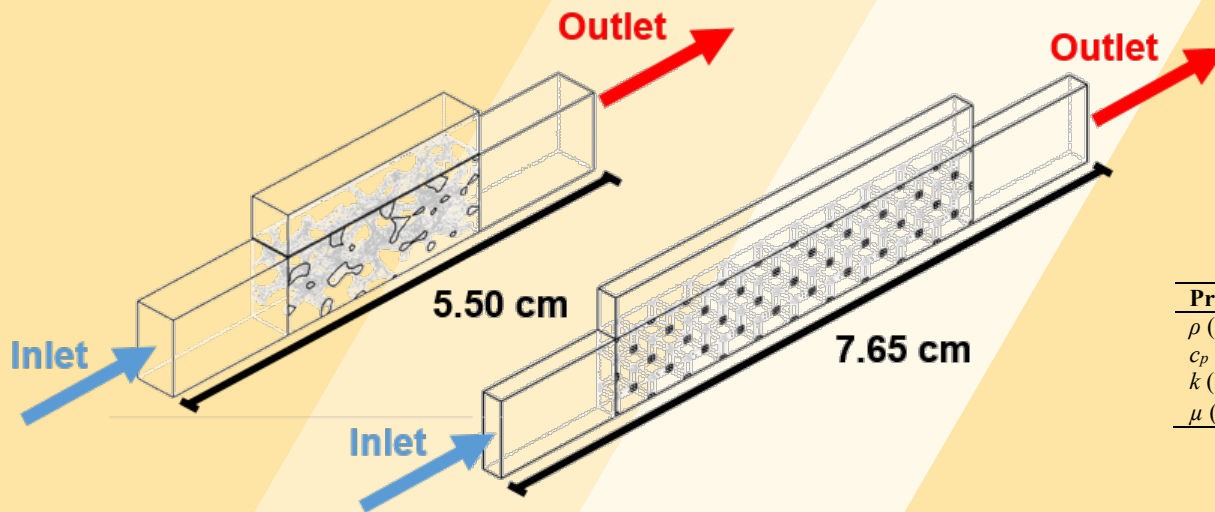


Table 2: Material properties at 25 °C .

Property	Al 6101	AlSi10Mg	Al 5083	Water
ρ (kg/m ³)	2700	2670	2660	998
c_p (J/kg•K)	896	890	900	4182
k (W/m•K)	167	173	117	0.6
μ (Pa•s)	-	-	-	0.001003

Figure 9: Reduced ERG sample geometry with TIM (left) and reduced AM geometry (right) used in computational studies.

3.2 Experimental testing setup and procedures

- Working fluid: degassed, deionized (DI) water
- Equipped with type-T thermocouples and several pressure transducers
- Uniform heat flux heating condition achieved with a heater block
- Test samples were nominally 4 cm x 10 cm x 0.93 cm
- Heated section area of 4 cm x 10 cm

Table 3: Experimental uncertainties.

Parameter	Uncertainty
Pressure	± 20 Pa
Flow rate	± 4 mL/s
Temperature (type T thermocouple)	± 0.5 K
Heat flux (heater block)	± 0.2 W/cm ²

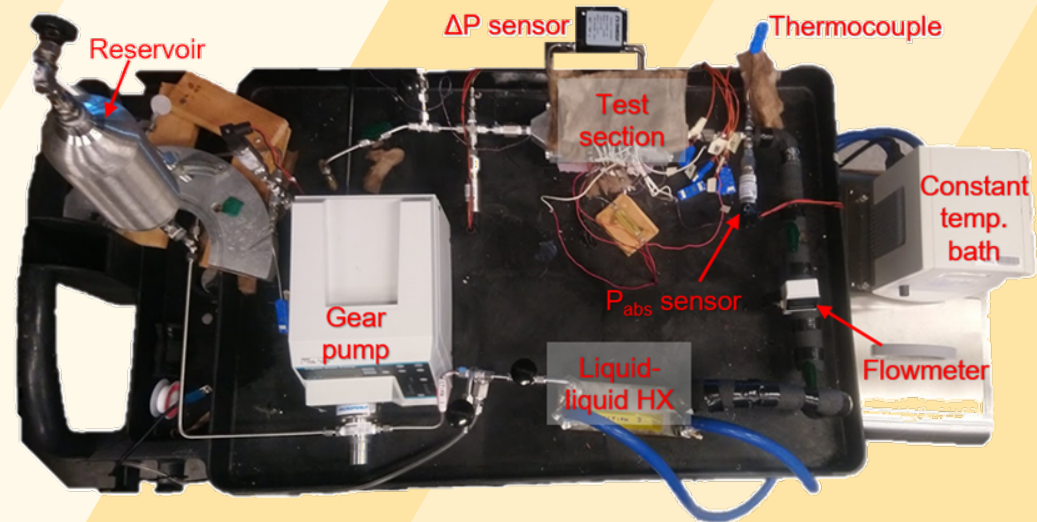
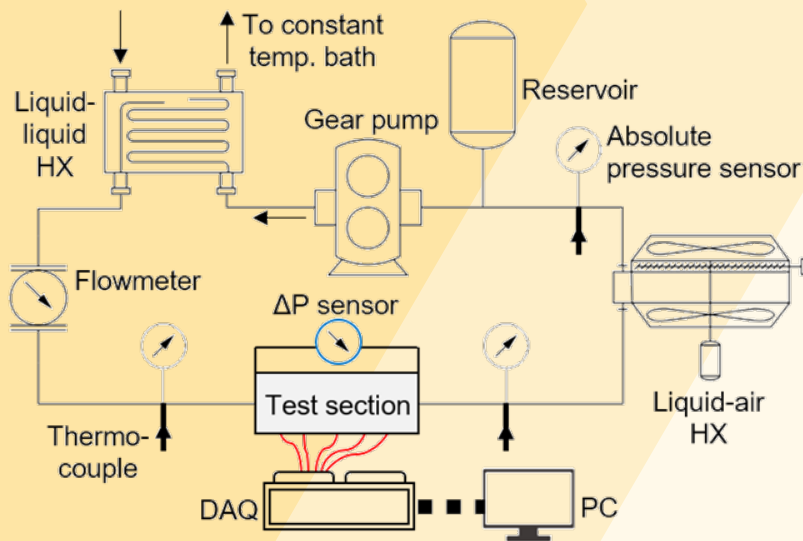


Figure 10: Closed flow loop and data acquisition setup.

- Validation before using computational models for further analysis
- Comparing total pressure drop across test section and effective Nusselt number
- Results fit to a second-order polynomial (Darcy-Forchheimer Law) and power law fit
- Good agreement between experimental and numerical results
- Pressure drop is higher (66%) for the AM sample, but the penalty comes with approximately 60% increase in effective heat transfer coefficient

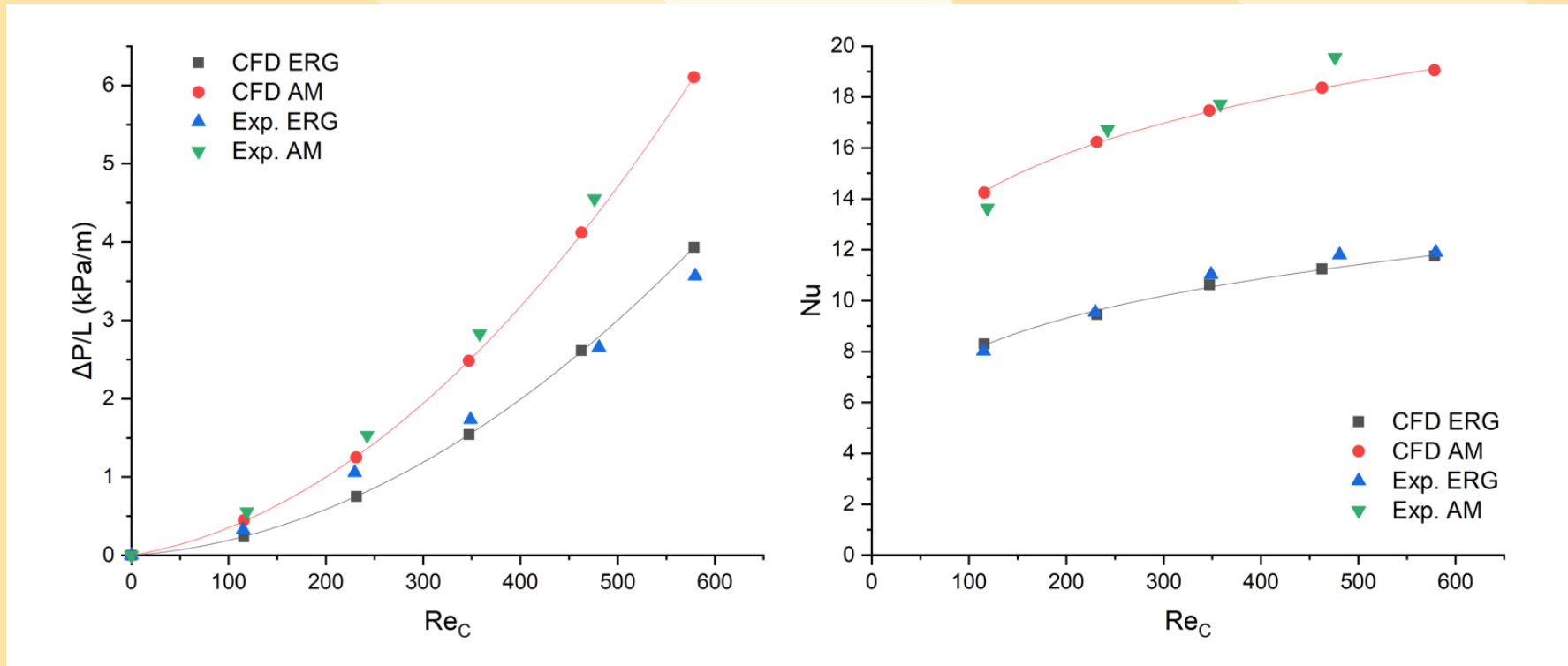


Figure 11: Reduced ERG sample geometry with TIM (left) and reduced AM geometry (right) used in computational studies.

4.2 Streamlines analysis for flow tortuosity studies

- Dispersion conductivity k_d accounts for pore-scale mixing in volume-averaged simulations
- Calmidi and Mahajan: $k_d = C_D \rho u \sqrt{K} c_p$
- Tortuosity defined as $\tau = s/L$
 - s is the total distance traveled
 - L is the shortest travel length possible
- Additional example correlation:

$$\frac{k_d}{k_f} = c(\tau - 1) \left(1 - \frac{\varepsilon}{\tau}\right) Re_p Pr$$
- Tortuosity values were calculated as 1.093 and 1.038, respectively
- Implies that commercial foam has higher thermal dispersion conductivity
- Further studies regarding k_d for either structure type should be undertaken

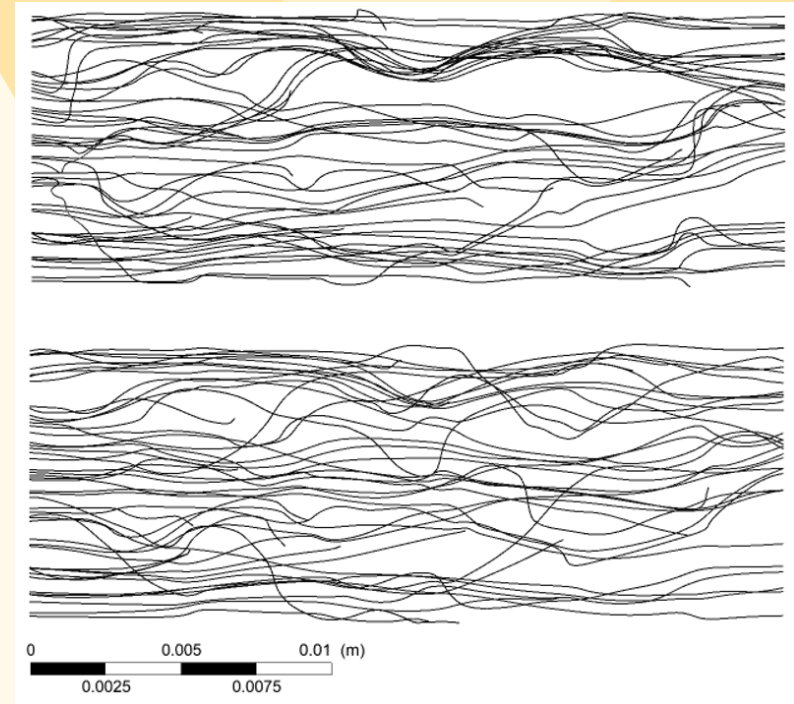


Figure 12: Streamlines visualized for stochastic geometry with $u = 2.5 \text{ cm/s}$ (top) and $u = 10 \text{ cm/s}$ (bottom)

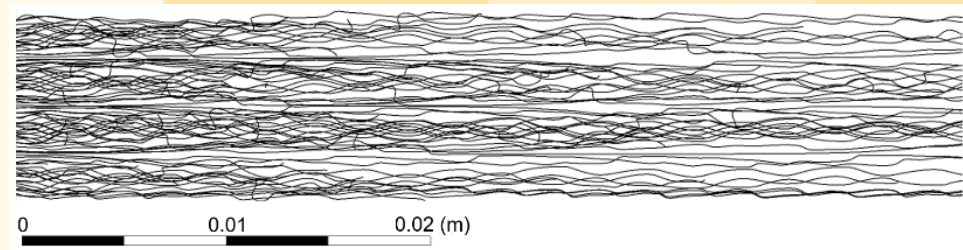


Figure 13: Designed sample streamlines for $u = 10 \text{ cm/s}$.

- Random vs. ordered flow patterns
- Existence of large stagnant zones in the commercial sample (with relative lack of such large low velocity zones in the AM geometry)

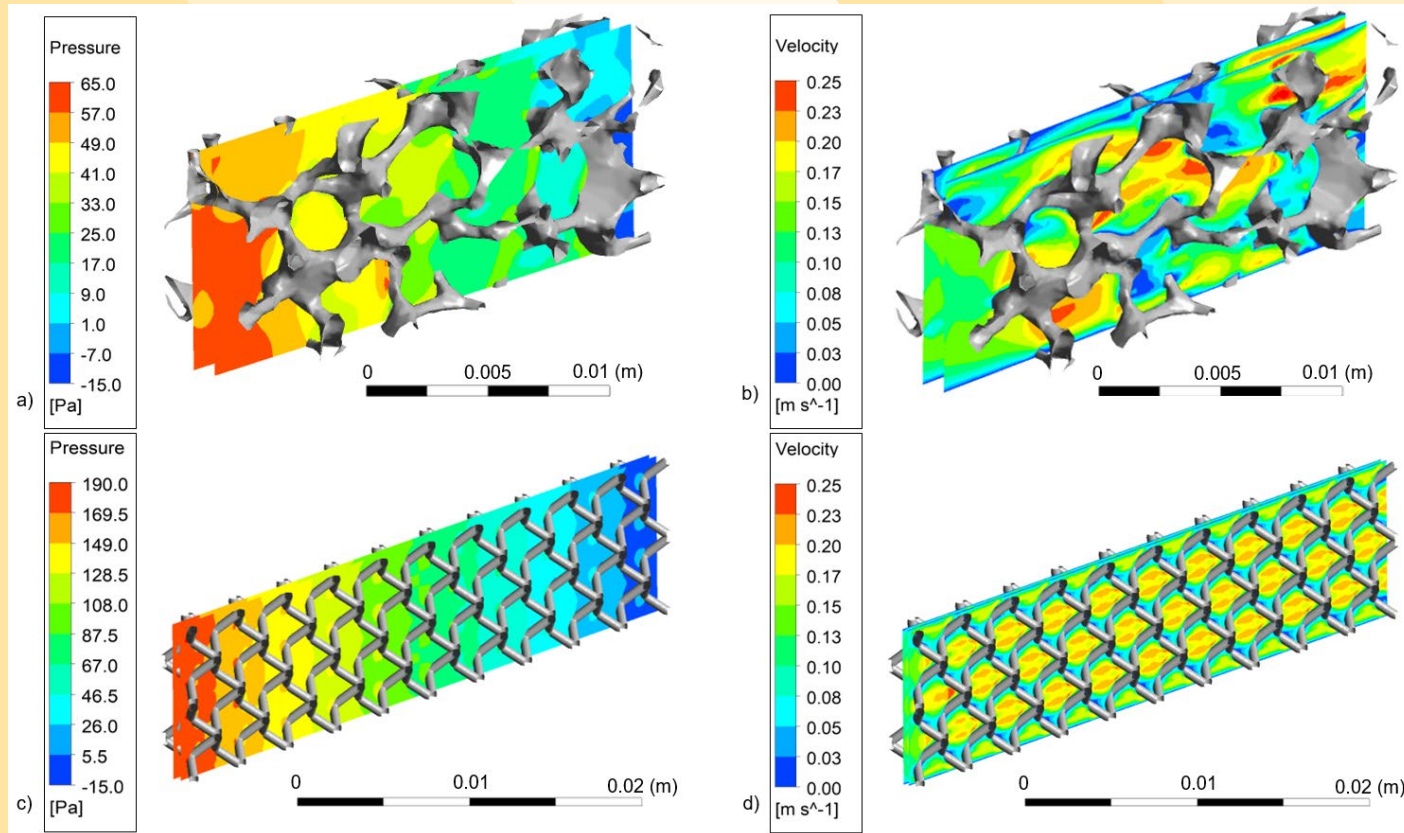


Figure 14: Flow fields for $u = 10 \text{ cm/s}$ for the commercial and AM foams a) Pressure contours, b) Velocity contours, c) Pressure contour, and d) Velocity contour for AM.

4.4 Resistor network for thermal interface material analysis

- Quantifying reasons for performance improvement – structural differences in the foam vs. elimination of the TIM
- U_{new} calculated for three k_{TIM} values ($k_{TIM} = 4.0, 40, \text{ and } \infty \text{ W/m}\cdot\text{K}$ to represent high conductivity epoxy, a solder, and no TIM layer)
- $U_{new} = \left[\frac{1}{U_{k=1.38}} - \frac{t_{TIM}}{k_{original}} + \frac{t_{TIM}}{k_{new}} \right]^{-1}$
- 1D resistor network validated with $k = 4.0 \text{ W/m}\cdot\text{K}$ results
- Incrementally improving k_{TIM} has a large impact at lower values but not so much at higher k values
- Performance of the commercial foam approaches AM foam with increasing flow speeds, which may be caused by the differences in k_d

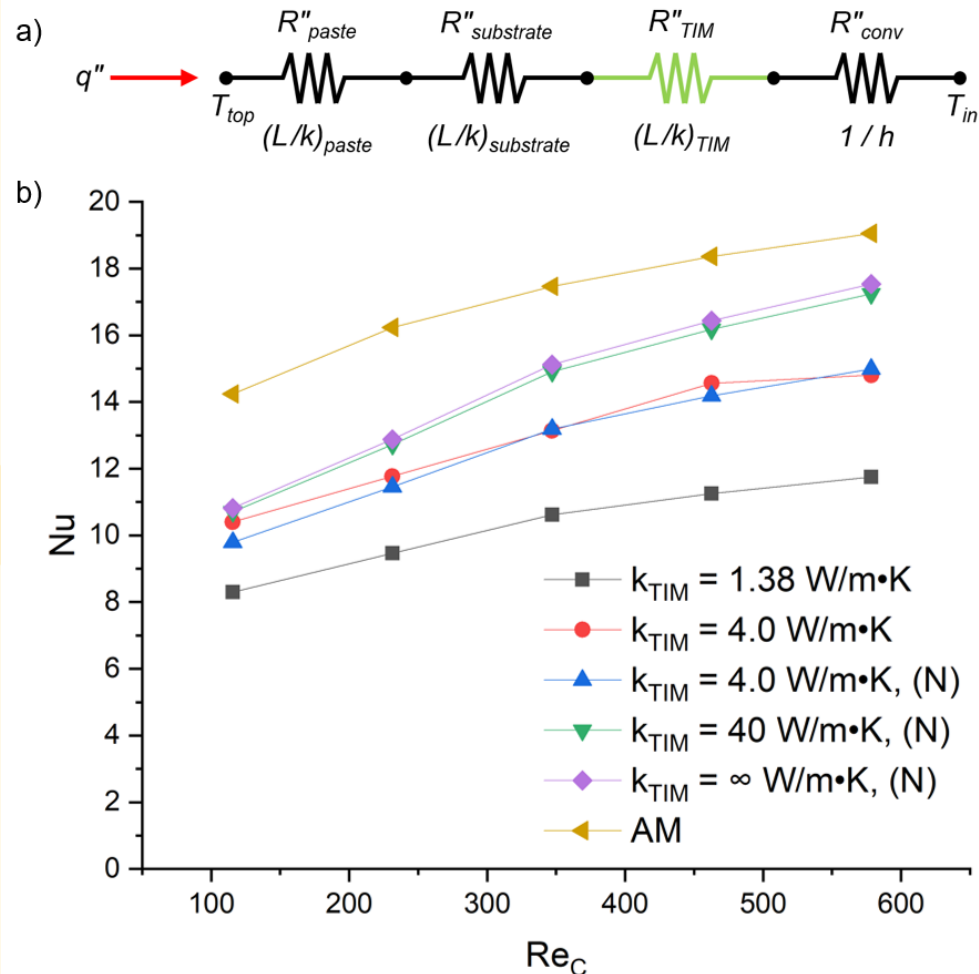


Figure 15: Non-dimensional heat transfer performance for AM foam and ERG Inc. foam with varying k_{TIM} values – (N) denotes values found using a resistance network approach.

4.5 Interfacial heat transfer coefficient and fin efficiency analysis

- Interfacial heat transfer coefficient (h_{sf}) is important for volume-averaged CFD simulations
- Calmidi and Mahajan: $Nu_{sf} = \frac{h_{sf}d_l}{k_f} = 0.52Re_l^{0.5}Pr^{0.37}$
- Hunt and Tien: $Nu_{sf} = \frac{h_{sf}d_l}{k_f} = 0.418Re_l^{0.53}Pr^{1/3}$
- Reasonable but not good agreement between correlations and numerical results
- Commercial foam has better fin efficiency except at lower inlet velocities – but this is due to the fact that the isothermal simulation convects much more heat for the AM model

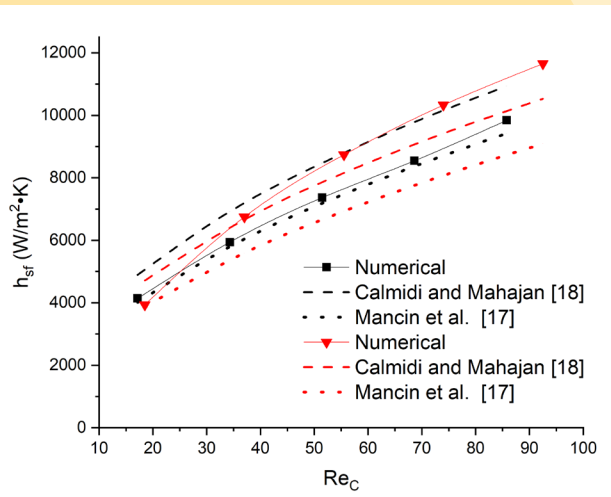


Figure 16: Comparison of numerical results and correlations results for commercial and AM foam

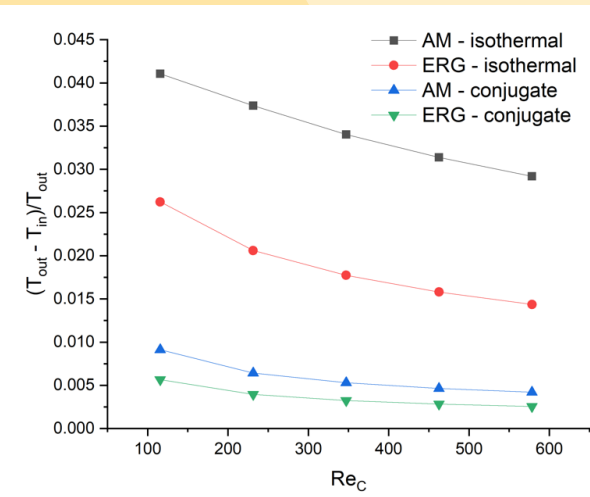
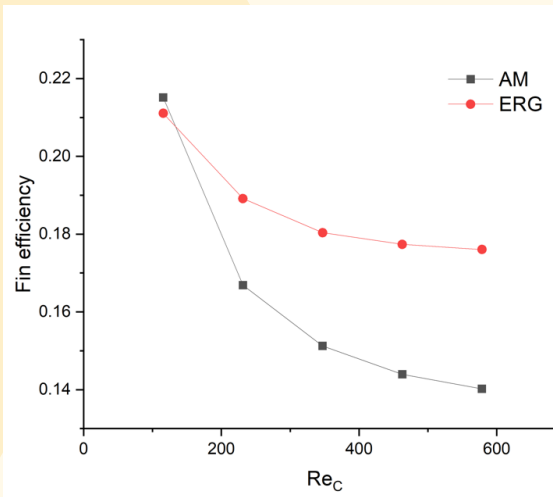


Figure 17: Fin efficiency for a 2.5 cm sample length (left) and nondimensionalized outlet temperature comparison for constant and variable ligament temperature (right).

- Demonstrated the advantages of traditionally manufactured and AM metal foams for thermal management
- Analyzed using commercial CFD-HT software, validated computational models
- Tortuosity results suggests that k_d should be adjusted for the AM structure
- Commercial foams would be viable if k_{TIM} values could be increased
- Interfacial heat transfer coefficients were shown to agree somewhat with correlations found in literature

Research Focus	2020				2021			
	Q1	Q2	Q3	Q4	Q1	Q2	Q3	Q4
Sample fabrication			Pressure mitigating structure					
Testing in flow loop				Pressure mitigating structure				
Conjugate heat transfer modeling	Pore scale boiling model		2 phase VA models			New structure 2 phase VA model validation		